

## 1 Steady State Tubular Reactor (Core)

1. Solve the steady state tubular reactor for 20 different Peclet numbers (between 0.01 and 100) and for a first ( $n=1$ ) and second ( $n=2$ ) order reaction. Use a Damköhler number of unity.

$$Pe = \frac{L^2/D}{L/v}, Da = \frac{L/v}{1/(kc_{in}^{n-1})} \quad (1)$$

- Complete the template `rhs.m` by implementing the non-linear equations to solve the problem.
2. Plot the conversion at the end of the reactor  $1 - c_{out}/c_{in}$  vs. Peclet number  $Pe$  for both reaction orders. Also, plot the ratio between the conversions of the first order and second order reaction.
    - What is better for these reactions, a lot of back-mixing (small  $Pe$ , CSTR) or ideal plug flow (large  $Pe$ , PFR)?
    - What influence does the reaction order have overall and at low or high Peclet numbers?
    - Complete the template `TubReact_steady_state.m`.

## 2 Dynamic Tubular Reactor (Core)

1. Solve the dynamic tubular reactor from time 0 to 5 with a MATLAB solver `ode23s`. Use the `rhs.m` from assignment 1 and the template `TubReact_dynamic.m`. Consider only a first order reaction with  $Pe = 100$  and  $Da = 1$ .
2. Plot the dimensionless concentration at the end of the reactor  $u_N$  vs. dimensionless time  $\theta$ 
  - At what time does the solution reach a steady state, i.e. how many reactor volumes of solvent will you need?
  - Complete the template `TubReact_dynamic.m`