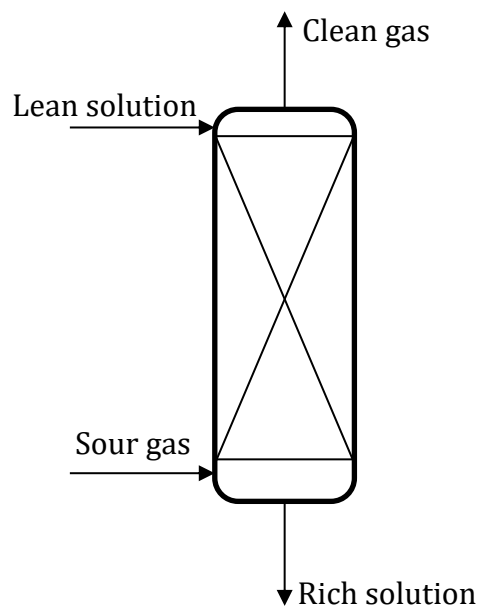


Separation Process Technology I

Aspen Tutorial 1: Absorption of H₂S with the Rectisol process

In this tutorial, we want to use a commercial software platform to perform the removal of hydrogen sulfide from a sour gas.

Let us consider the following configuration:



Where the entering sour gas is specified as follow:

- Composition, [mole frac.]
CO₂ 0.0302
H₂S 0.0019
CO 0.5886
N₂ 0.0977
H₂ 0.2722
AR 0.0094
- Pressure: 40 bar
- Flow rate: 50 kg/s
- Temperature: -10°C

The chosen process for H₂S removal is the Rectisol Process.

It is required to:

- I. Develop an equilibrium-based Aspen simulation for the considered process and:
 - a. Identify the L/G that leads to the specification $H_2S_{\text{cleangas}} = 0.1\text{ppm}$.
 - b. Investigate the effects of the temperature in the lean solution when the specification $H_2S_{\text{cleangas}} = 0.1\text{ppm}$ is kept constant
- II. Develop a rate-based Aspen simulation and:
 - a. Investigate how the packing height and the L/G affect the system and identify the design conditions for which the specification $H_2S_{\text{cleangas}} = 0.1\text{ppm}$ is guaranteed.

Assumptions for the simulations:

Property method: PC-SAFT (Perturbated Chain Statistical Association Fluid Theory)

5 equilibrium stages

Temperature range for task I.b: $T_{\min} = -60\text{ }^\circ\text{C}$ $T_{\max} = -20\text{ }^\circ\text{C}$

Packing type for task II:

Type: INTX

Vendor: generic

Material: ceramic

Dimension: 50mm

Fractional approach to maximum capacity: 0.6