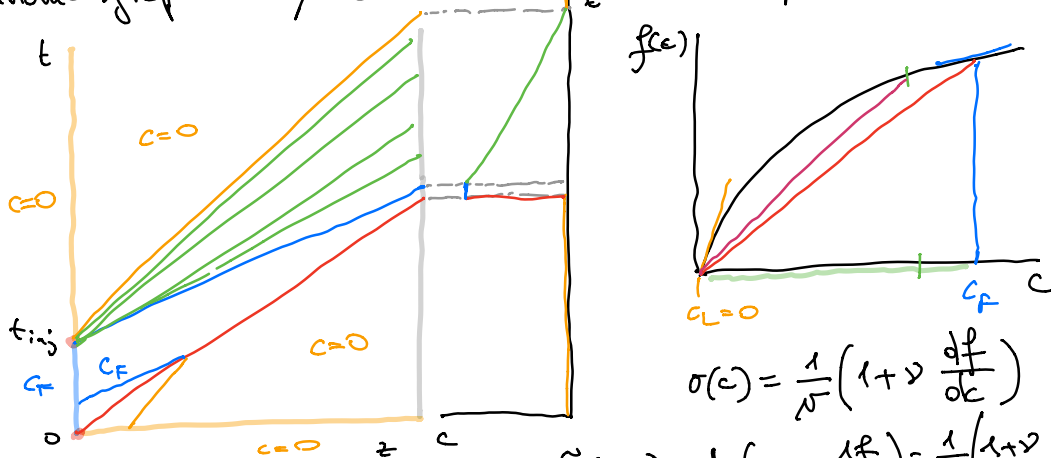


1 Chromatographic cycle : initial value problem



$$\sigma(c) = \frac{1}{v} \left(1 + v \frac{df}{dc} \right)$$

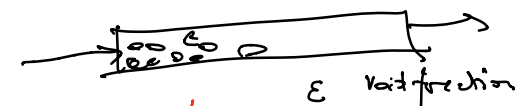
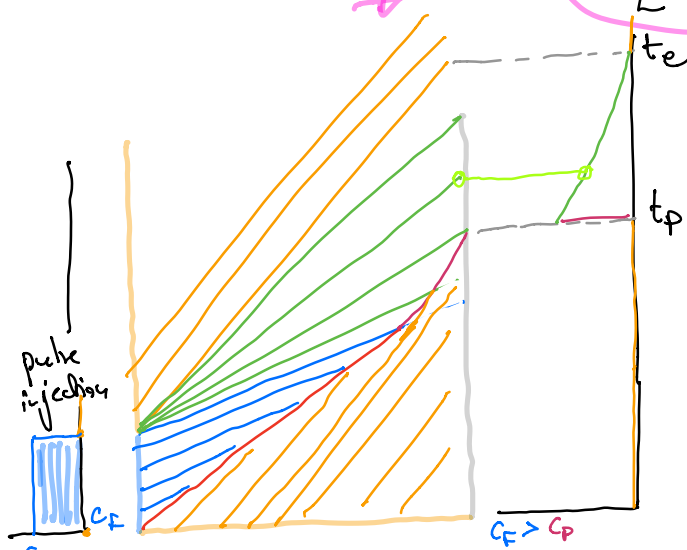
$$\tilde{\sigma}(c_F, 0) = \frac{1}{v} \left(1 + v \frac{df}{dc} \right) = \frac{1}{v} \left(1 + v \frac{f'(c_F)}{c_F} \right)$$

blue: $t = t_{inj} + \sigma(c_F) z$ ⊕
 red: $t = \tilde{\sigma} z$ ⊖

$$0 = t_{inj} + (\sigma_F - \tilde{\sigma}) z = t_{inj} + \frac{v}{v} \left(f'(c_F) - \frac{f(c_F)}{c_F} \right) z$$

$$\Rightarrow z = \frac{t_{inj} v}{v} \left(\frac{f(c_F)}{c_F} - f'(c_F) \right)^{-1} < L$$

$\frac{t_{inj} v}{L} < v \left(\frac{f(c_F)}{c_F} - f'(c_F) \right)$ for interaction



$c_p ?$ $t_p ?$

square pulse overall material balance

$$IN = \cancel{Q c_F t_{inj}} = \cancel{Q} \int_{t_p}^{t_e} c(t) dt = OUT =$$

$$t = \sigma(c) L = \frac{L}{v} \left(1 + v f'(c) \right)$$

$$dt = \frac{L}{v} v f''(c) dc$$

$$= \frac{Lv}{\sigma} \int_{c_p}^0 c f''(c) dc = c_p \tau_{inj}$$

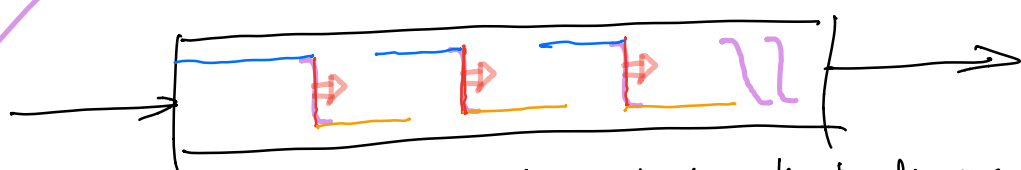
$$\int_{c_p}^0 c f''(c) dc = \left[c f'(c) \right]_{c_p}^0 - \int_{c_p}^0 f'(c) dc = \left[c f'(c) - f(c) \right]_{c_p}^0 = f(c_p) - c_p f'(c_p)$$

$$f(c_p) = \frac{H c_p}{\lambda + K c_p}$$

$$f'(c_p) = \frac{H}{(\lambda + K c_p)^2}$$

$$\frac{K H c_p^2}{(\lambda + K c_p)^2}$$

2 Constant pattern



smooth concentration front, traveling at constant velocity, without changing shape

challenge: can we model a constant pattern?

Equilibrium theory (method of characteristics) →

- Ans 1: no mass transfer resistances = phase equilibrium
- Ans 2: transport through convection only (no diffusion)

$$\frac{\partial}{\partial t} (\epsilon c + (1-\epsilon) f(c)) + \epsilon v \frac{\partial c}{\partial z} = 0$$

Ratz model of chromatography: (1) $n \neq f(c)$

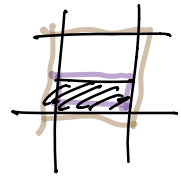
(2) $F = u c - \epsilon D \frac{\partial c}{\partial z}$

convection ↑ diffusion ↑

$$\frac{\partial}{\partial t} (\epsilon c + (1-\epsilon)m) + \epsilon v \frac{\partial c}{\partial z} = \epsilon D \frac{\partial^2 c}{\partial z^2}$$

$$\frac{\partial m}{\partial t} = q_p k (f(c) - m)$$

$\left[\frac{m^2}{m^3} \right]$ $\left[\frac{m}{s} \right]$



$$\frac{\partial c}{\partial z} + v \frac{\partial m}{\partial c} + \frac{\partial c}{\partial x} = \frac{1}{Pe} \frac{\partial^2 c}{\partial x^2}$$

$$\frac{\partial m}{\partial c} = St (f(c) - m)$$

Eq. Theory

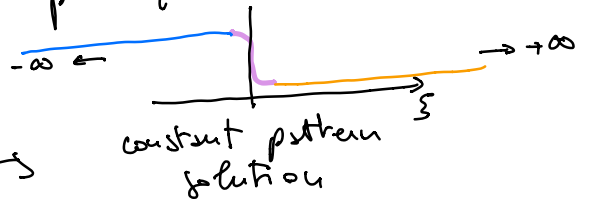
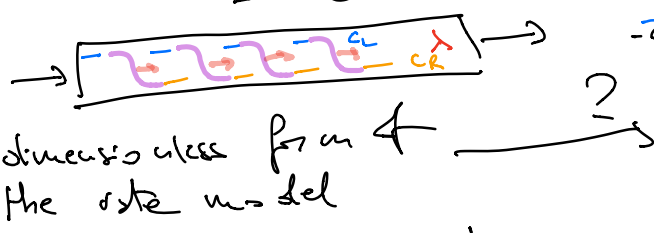
$$\frac{\partial m}{\partial t} = \frac{df}{dc} \frac{\partial c}{\partial t}$$

$$\tau = \frac{L}{v} \quad x = \frac{z}{L} \quad v = \frac{1-\epsilon}{\epsilon}$$

$$Pe = \frac{L^2/D}{L/v} = \frac{\text{char. diffusion time}}{\text{residence time}} \quad St = \frac{L/v}{1/(q_p k)} = \frac{\text{residence time}}{\text{char. mass transfer time}}$$

Equilibrium theory is the limit for:

- $Pe \rightarrow \infty$ no diffusion
- $St \rightarrow \infty$ phase equilibrium



- Assumptions
- (1) constant velocity: v
 - (2) infinitely long column
 - (3) moving coordinate system

$$- \infty < x < + \infty$$

$$\xi = x - vt$$

$$\frac{\partial c}{\partial \xi} = c'$$

$$\frac{\partial^2 c}{\partial \xi^2} = c''$$

$$\frac{\partial}{\partial x} = \frac{d}{d\xi} \frac{\partial \xi}{\partial x} = \frac{d}{d\xi}$$

$$\frac{\partial^2}{\partial x^2} = \frac{d^2}{d\xi^2}$$

$$\frac{\partial}{\partial t} = \frac{d}{d\xi} \frac{\partial \xi}{\partial t} = -v \frac{d}{d\xi}$$

(4) B.C. $\xi \rightarrow -\infty$ $c \rightarrow c_L$ $\xi \rightarrow +\infty$ $c \rightarrow c_R$

$c', c'' \rightarrow 0$

3

$$\begin{cases} -\lambda c' - \nu \lambda m' + c' = \frac{1}{Pe} c'' \\ -\lambda m' = St(f-m) \end{cases}$$

PDEs \rightarrow ODEs
 (7,2) (5)
 $f = f(c)$

$$\begin{cases} \nu m = \frac{1}{\lambda} [c'(1-\lambda) - c''/Pe] \\ c'(1-\lambda) + \nu St(f-m) = c''/Pe \end{cases} \leftarrow \text{this determines } m!$$

$\frac{d}{d\xi}$

$$c''(1-\lambda) + \nu St(f' - m') = c'''/Pe$$

$$c''(1-\lambda) + \nu St f' = \frac{St}{\lambda} [c'(1-\lambda) - c''/Pe] + c'''/Pe \quad \text{in } c \text{ only!}$$

$$\frac{1}{Pe St} c''' - \left(\frac{1}{\lambda Pe} + \frac{1-\lambda}{St} \right) c'' + \frac{1-\lambda}{\lambda} c' - \nu f' = 0 \rightarrow c$$

λ is unknown !!

(4)