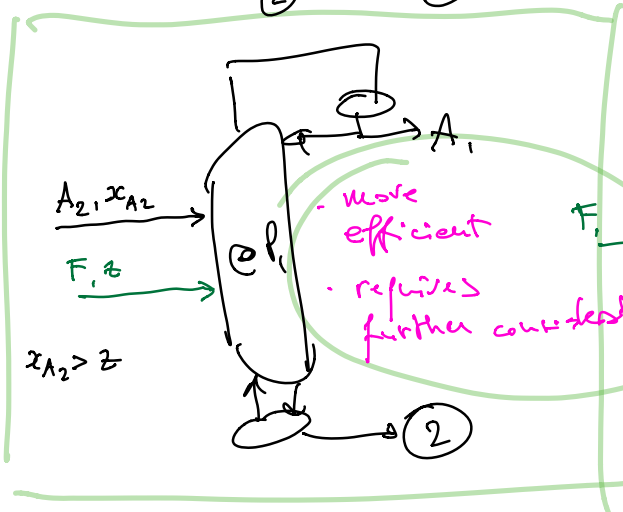
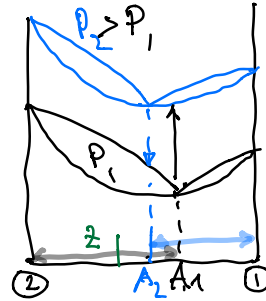
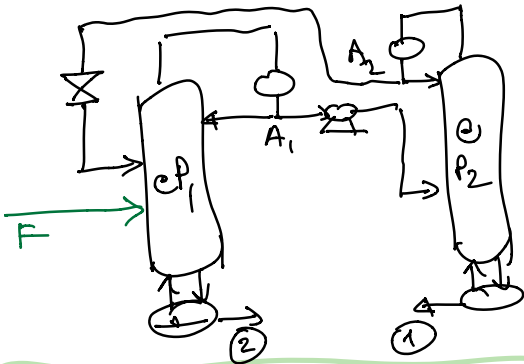
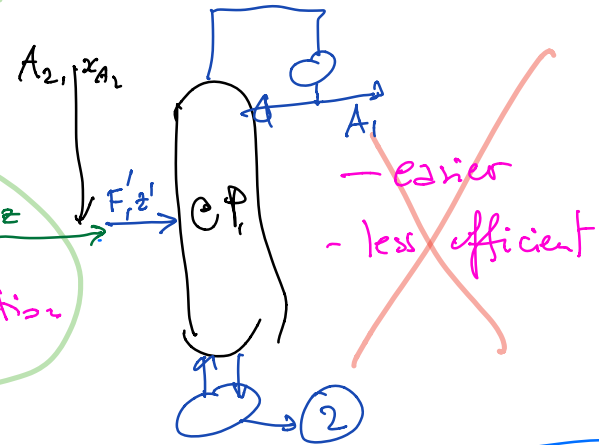


Homogeneous azeotropic distillation

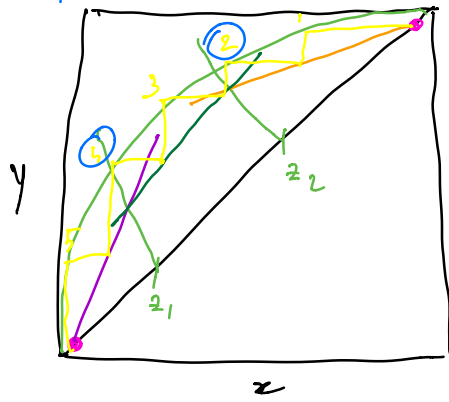
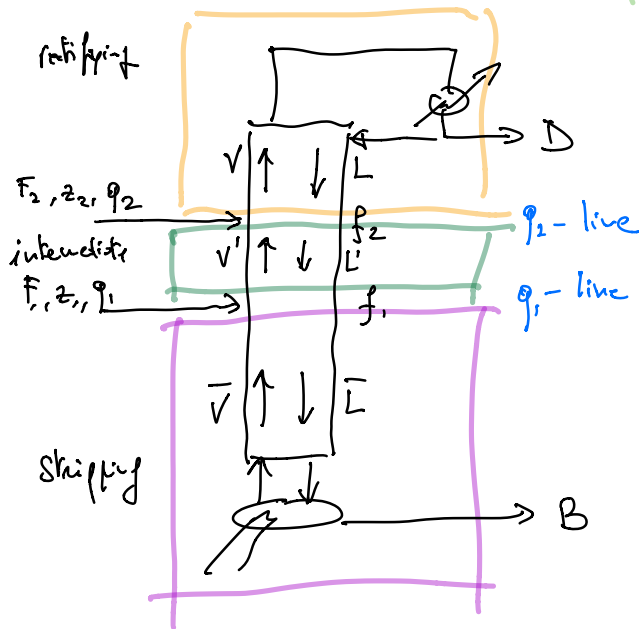


more efficient  
requires further condensation



— easier  
— less efficient

Distillation w/ multiple feeds

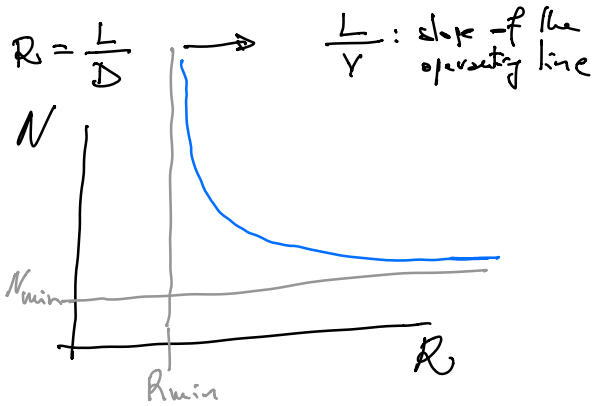
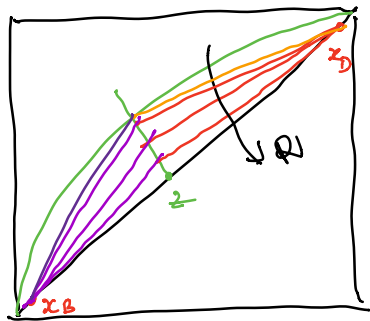


# Multicomponent distillation

- 1 From binary to multicomponent
- 2 Features of multicomponent distillation
- 3 Introduction to how to calculate  $N_{min}$  and  $R_{min}$
- 4 Fenske method  $\rightarrow N_{min}$  based on  $R \rightarrow \infty$
- 5 Underwood method  $\rightarrow R_{min}$  based on  $N \rightarrow \infty$
- 6 Gilliland diagram

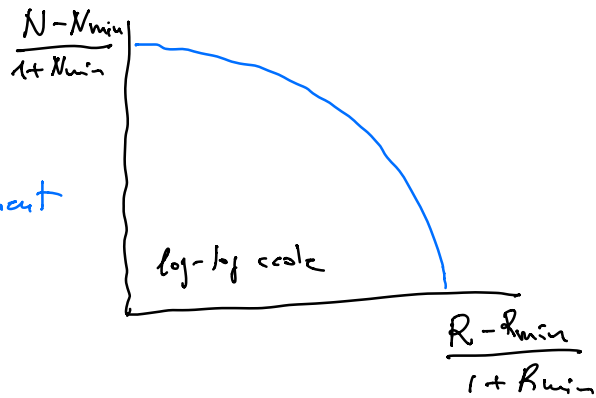
$\rightarrow$  short-cut design of multicomponent distillation  
 $\rightarrow$  basis for "Aspen Plus simulation"

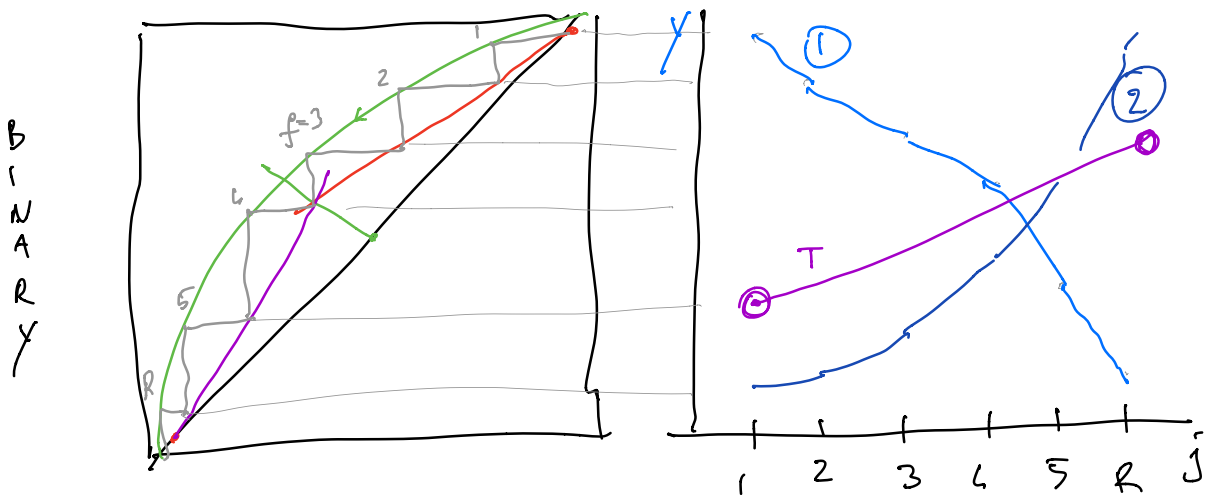
## 1 The Colburn-Thiele method



6  
3

Gilliland diagram  
 $\rightarrow$  binary  
 $\rightarrow$  multicomponent

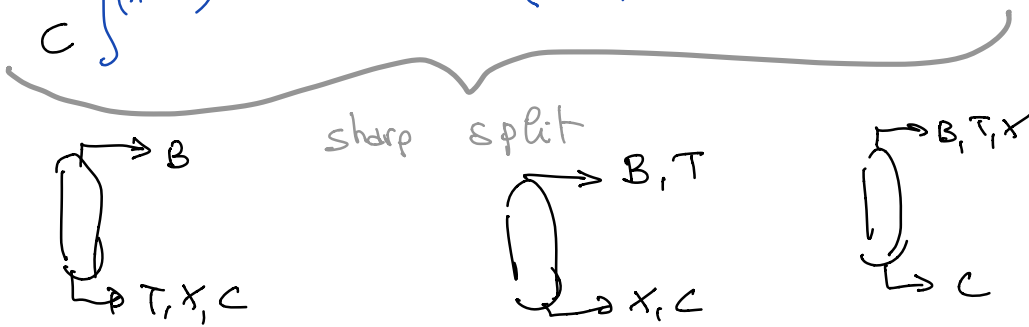


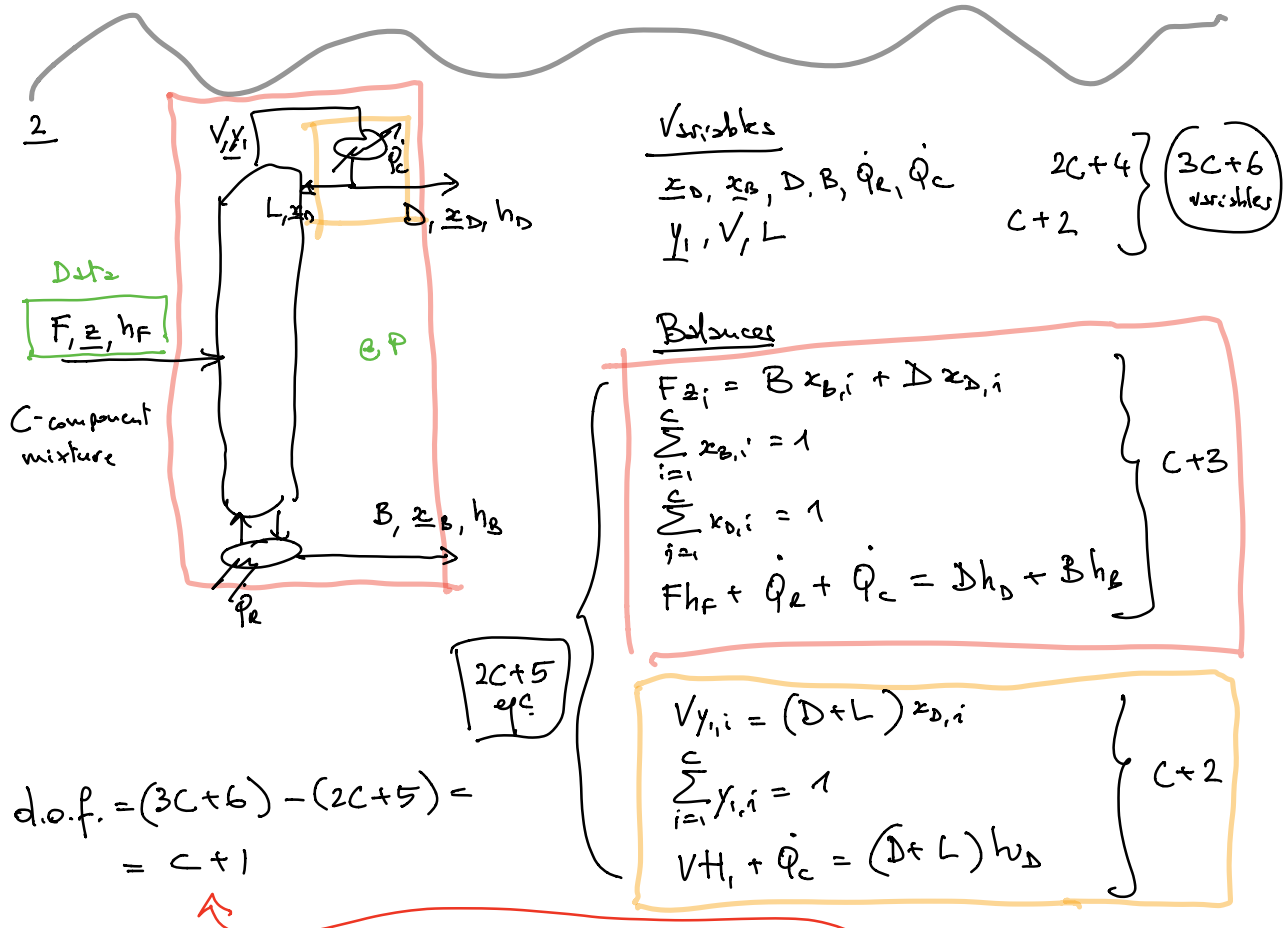
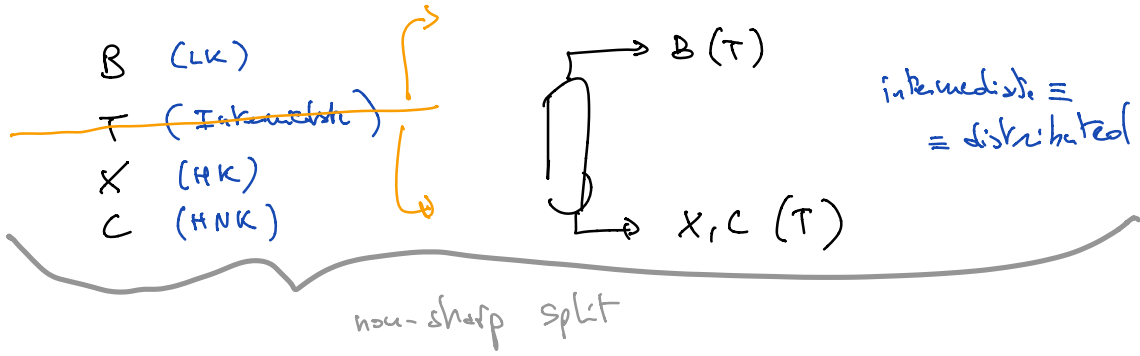


Multicomponent mixture

|                             |             |             |               |                             |            |
|-----------------------------|-------------|-------------|---------------|-----------------------------|------------|
| ↑<br>vol. fraction          | Benzene     | $C_6H_6$    |               | $80^\circ C$                | ↓<br>$T_b$ |
|                             | Toluene     | $C_7H_8$    |               | $111^\circ C$               |            |
|                             | Xylene      | $C_8H_{10}$ |               | $138^\circ C - 144^\circ C$ |            |
|                             |             |             |               |                             |            |
|                             |             |             |               |                             |            |
| Styrene (isopropyl benzene) | $C_9H_{12}$ |             | $152^\circ C$ |                             |            |

|        |               |               |               |
|--------|---------------|---------------|---------------|
| ↓<br>D | <u>B</u> (LK) | B (LNK)       | B } LNK       |
|        | T (HK)        | <u>T</u> (LK) | T } LNK       |
|        | X } (HNK)     | X (HK)        | <u>X</u> (LK) |
|        | C } (HNK)     | C (HNK)       | C (HK)        |





Specs:  $R = L/D$ ,  $x_{D,LK}$ !,  $x_{B,HK}$ !

3 specs

$C+1 - 3 = C-2$  missing conditions

How to design specs on LK and HK

$$\frac{F_{z,i}}{F_{z,i}} = \frac{B x_{B,i} + D x_{D,i}}{F_{z,i}} \Rightarrow 1 = \frac{B x_{B,i}}{F_{z,i}} + \frac{D x_{D,i}}{F_{z,i}}$$

FR: fractional recovery

$$1 = FR_i^B + FR_i^D$$

Specs:  $R = \frac{L}{D}$ ,  $FR_{LK}^D$ ,  $FR_{HK}^B$

sharp split



$$\begin{aligned} FR_{LNK}^D &= 1 \\ FR_{LK}^D &= 0.98 \\ FR_{HK}^B &= 0.99 \\ FR_{HNK}^B &= 1 \end{aligned}$$

C component, LK + HK

C-2 NK component

All missing conditions are not missing separate

non-sharp split



$$\begin{aligned} FR_{LNK}^D &= 1 \\ FR_{LK}^D &= 0.99 \\ FR_I^D &= ?? \\ FR_{HK}^B &= 0.95 \\ FR_{HNK}^B &= 1 \end{aligned}$$

C-2 - Intermediate

We are still missing conditions!

L.V.E. for C components

$f_i^L = f_i^V$  isoperficiency (ideal gas + unideal liquid)

$$y_i = \frac{p_i^V(\tau) x_i}{P} \quad y_i(T, P, \underline{x}) = \frac{p_i^V(\tau) \gamma_i}{P} x_i = K_i(T, P, \underline{x}) x_i$$

$$y_i = K_i x_i$$

relative volatility:  $\alpha_{i2} = \frac{y_i/x_i}{y_2/x_2} = \frac{K_i(T, P, \underline{x})}{K_2(T, P, \underline{x})}$

$$y_i = \alpha_{i2} K_2 x_i$$

$$\sum_{i=1}^C y_i = 1 = K_2 \sum_{i=1}^C \alpha_{i2} x_i \Rightarrow K_2 = \frac{1}{\sum_{i=1}^C \alpha_{i2} x_i}$$

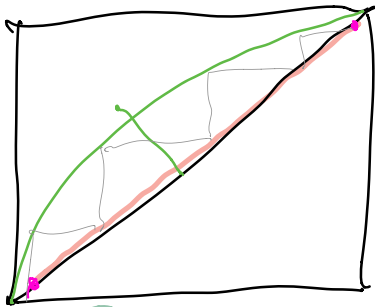
$$y_i = \frac{\alpha_{i2} x_i}{\sum_{i=1}^C \alpha_{i2} x_i}$$

$$\alpha_{i2} = \text{constant}$$

$$\alpha_{i2} = \frac{K_i(\tau, P, z)}{K_2(\tau, P, z)} = \frac{p_i^v(\tau) \delta_i}{p_2^v(\tau) \delta_2} \stackrel{\delta_i \approx 1}{=} \frac{p_i^v(\tau)}{p_2^v(\tau)} \approx \text{const.}$$

C.P. V.  $\alpha_{i2}$  ist konstant

$$y_i = \frac{\alpha_{i2} x_i}{\sum_{i=1}^C \alpha_{i2} x_i}$$



Fenske  $\Rightarrow$  N min

$$\Rightarrow R \rightarrow \infty$$

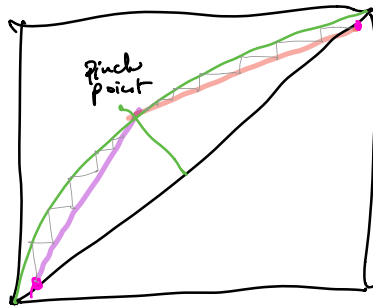
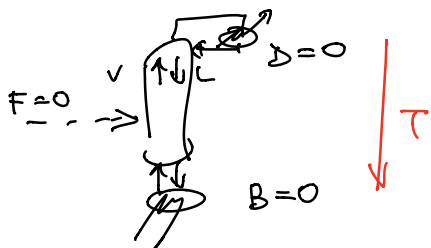
$$\Rightarrow \frac{L}{D} \rightarrow \infty$$

$$V = L + D$$

$$\Rightarrow L = V$$

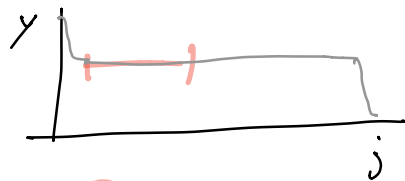
$$\Rightarrow C = \bar{V}$$

$$\left. \begin{matrix} D=0 \\ B=0 \end{matrix} \right\} \Rightarrow F=0$$



Underwood  $\Rightarrow$  N min

$$\Rightarrow N \rightarrow \infty$$



reclipping  $x_{j,i} = x_{j+1,i} \dots$

stripping  $x_{k,i} = x_{k+1,i} \dots$

pinch-point