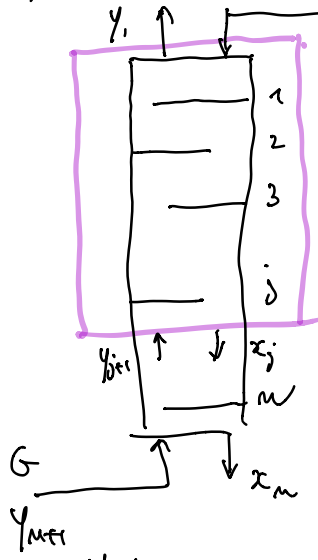


(I) Design of a countercurrent absorber



$$\alpha = \frac{y_{n+1} - y_1}{y_{n+1} - y_0^*} = \frac{A^{n+1} - A}{A^{n+1} - 1} = \alpha$$

absorption efficiency

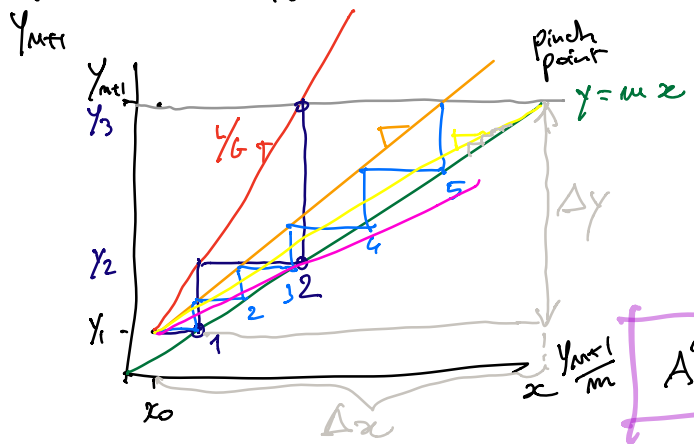
$$y_0^* = m x_0$$

$$A = \frac{L/G}{m} \quad \text{- operating parameter}$$

min-site - operating condition: A

absorption efficiency α

Kremser equation



Data

$G, y_{n+1}, x_0, m(T, P)$

Specification

$y_1 \geq y_1^{max}$

$$A^{n+1} (1 - \alpha_{min}) - A + \alpha_{min} = 0$$

① $n, A \rightarrow \alpha \rightarrow y_1 = y_{n+1} - \alpha (y_{n+1} - y_0^*)$

② $\alpha_{min} (y_1^{max}), A \rightarrow n$

③ $\alpha_{min}, n \rightarrow A$ numerical solution

$$n = \frac{1}{\ln A} \ln \left(\frac{1 - \frac{\alpha_{min}}{A}}{1 - \alpha_{min}} \right)$$

$$A^n (1 - \alpha_{min}) = 1 - \frac{\alpha_{min}}{A}$$

$$A_{min} = \alpha_{min}$$

L/G (or A) \downarrow n \uparrow

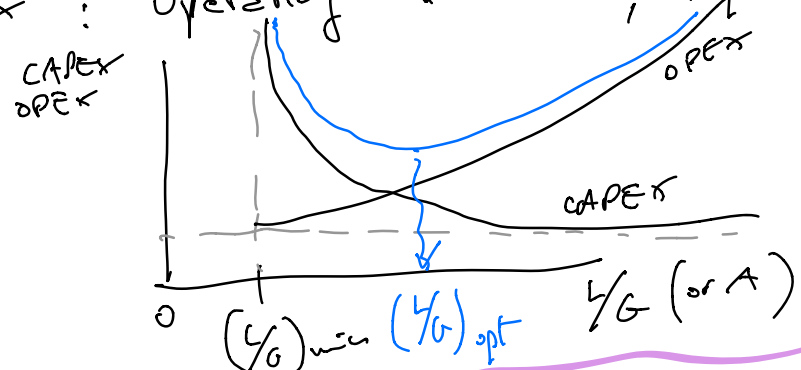
$$\left(\frac{L}{G}\right)_{min} = \frac{\Delta y}{\Delta x} = \frac{y_{n+1} - y_1}{y_{n+1}/m - x_0} = \frac{m(y_{n+1} - y_1)}{y_{n+1} - y_0^*}$$

①

minimum L/G ratio, that depends on the problem (y_{in}, x_0, y_1^{max}) and on thermodynamics (m)

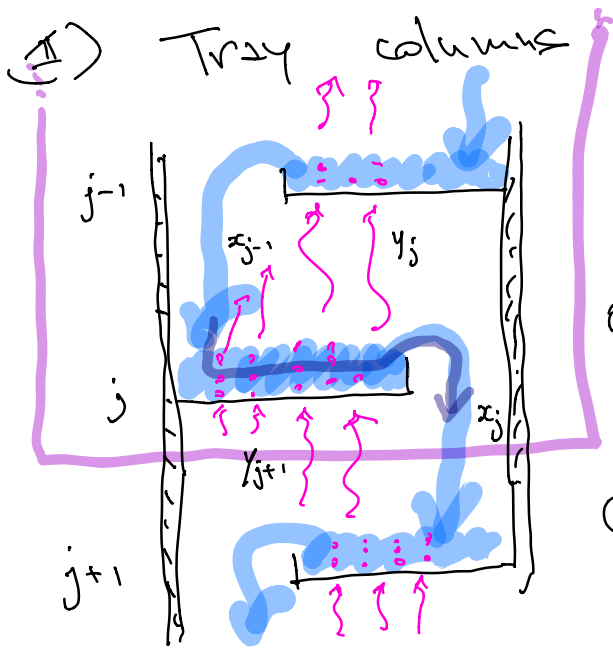
$\hookrightarrow n \rightarrow \infty \Rightarrow A > A_{min} ?!$
 cost optimisation \nearrow

CAPEX: Capital Expenditures, depend on m
 OPEX: Operating, depend on A



Data (y_{in}, G, x_0, m) + Specs $(y_1^{max} \rightarrow d_{min}) \rightarrow$
 $\rightarrow A_{min} (= d_{min}) \rightarrow A > A_{min} \rightarrow L/G (= Am) \rightarrow$
 ② $\rightarrow n^* (n^* \in \mathbb{R}) \rightarrow n^* < n < n^* + 1 \rightarrow$
 ① $\rightarrow d > d_{min} \rightarrow y_1 < y_1^{max} \xrightarrow{\text{overall inst. bal.}} x_m$

$$G y_{in} + L x_0 = G y_1 + L x_m$$



Eq. stage $y_j = m x_j$

Stage n-f.-at-equilibrium

① mat. balance

$$G y_{j+1} + L x_j = G y_j + L x_{j+1}$$

② eq. condition

$$y_j^* = m x_j$$

③ stage efficiency (Murphree)

$$E_j^{MG} = \frac{y_{j+1} - y_j}{y_{j+1} - y_j^*}$$

$E_j^{NG} = E < 1$ output

$$y_j = y_{j+1} (1-E) + E y_j^*$$

$$\Rightarrow y_{j+1} = A' y_j + B' (y_i - A y_0^*)$$

$E=1 \rightarrow$ eq. stages

$$A' = \frac{A}{E+A-EA}$$

$$B' = \frac{E}{E+A-EA}$$

when $E=1$

$$A' = A$$

$$B' = 1$$

$$j=0 \quad y_0 = y_{j+1} (1-E) + E y_0^*$$

$$y_j = \left[y_1 (1-E) + E y_0^* - \frac{B'}{1-A'} (y_1 - A y_0^*) \right] (A')^j + \frac{B'}{1-A'} (y_1 - A y_0^*)$$

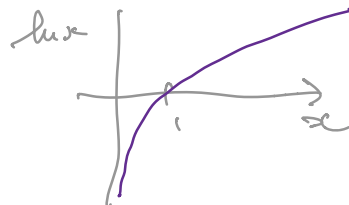
$$j = n+1 \rightarrow$$

$$y_{n+1} \rightarrow$$

$$\alpha = \frac{y_{n+1} - y_1}{y_{n+1} - y_0^*} \quad \text{is always } > 1$$

$$\alpha = \frac{(A')^{n+1} - 1}{(A')^{n+1} - 1/A}$$

generalised Kremser eq.



$$m' = \frac{1}{\ln A'} \ln \left(\frac{1 - \frac{d_{min}}{A}}{1 - d_{min}} \right)$$

$$A_{min} = d_{min}$$

$$\frac{m}{m'} = \frac{\ln A'}{\ln A} < 1 \rightarrow$$

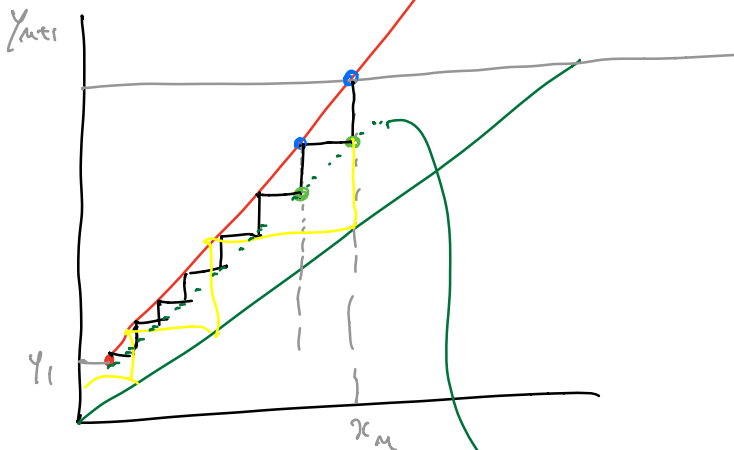
$$1 < A' < A$$

$$A < A' < 1$$

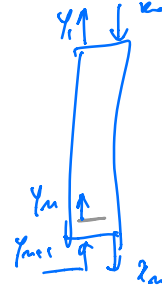
these are the only

cases when $A' = \frac{A}{E+A-EA}$

$$m' (E < 1) > m (E = 1)$$



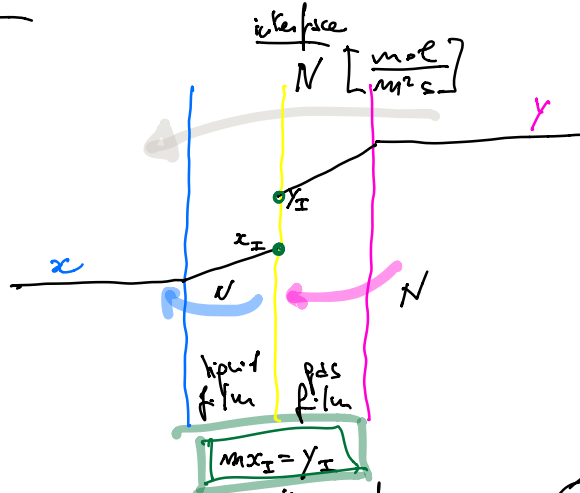
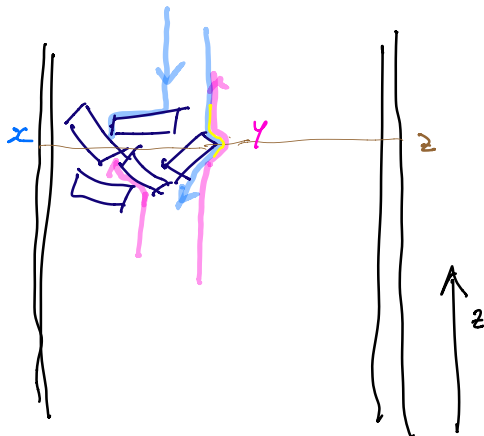
$$D.L = E = \frac{y_{i+1} - y_j}{y_{i+1} - y_j^*} < 1$$



pseudo-equilibrium line

∞ ∞

(14) Packed columns



ep. thermodynamic at the interface

4

$$N = k_G (y - y_I) = k_L (x_2 - x)$$

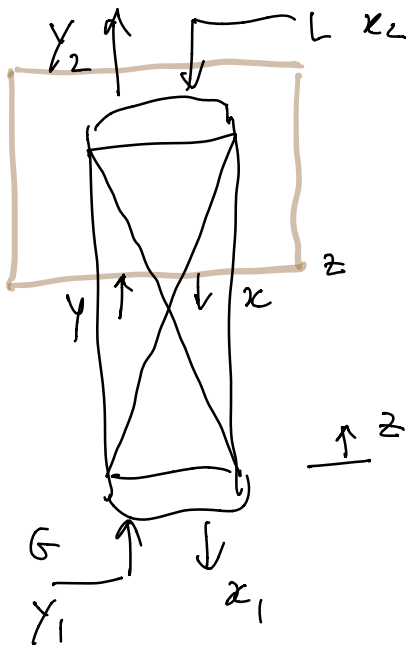
$$\frac{N}{k_G} = y - y_I \quad m \frac{N}{k_L} = m(x_2 - x) = y_I - mx = y_I - y^*$$

$$N \left(\frac{1}{k_G} + \frac{m}{k_L} \right) = y - y^*$$

$$\frac{1}{K_G} = \frac{1}{k_G} + \frac{m}{k_L}$$

$$N = K_G (y - y^*) = k_G (y - mx)$$

2-film theory



①

$$Gy + Lx_2 = Gy_2 + Lx$$

②

$$y^* = mx$$

③

mass transfer

01.06.2021

$$Py = H(\tau) x$$

$$y = \frac{H(\tau)}{P} x$$

$$y = mx$$

Henry's law

$H(\tau)$ Henry's constant

$$m = \frac{H(\tau)}{P} : \text{any nomenclature}$$